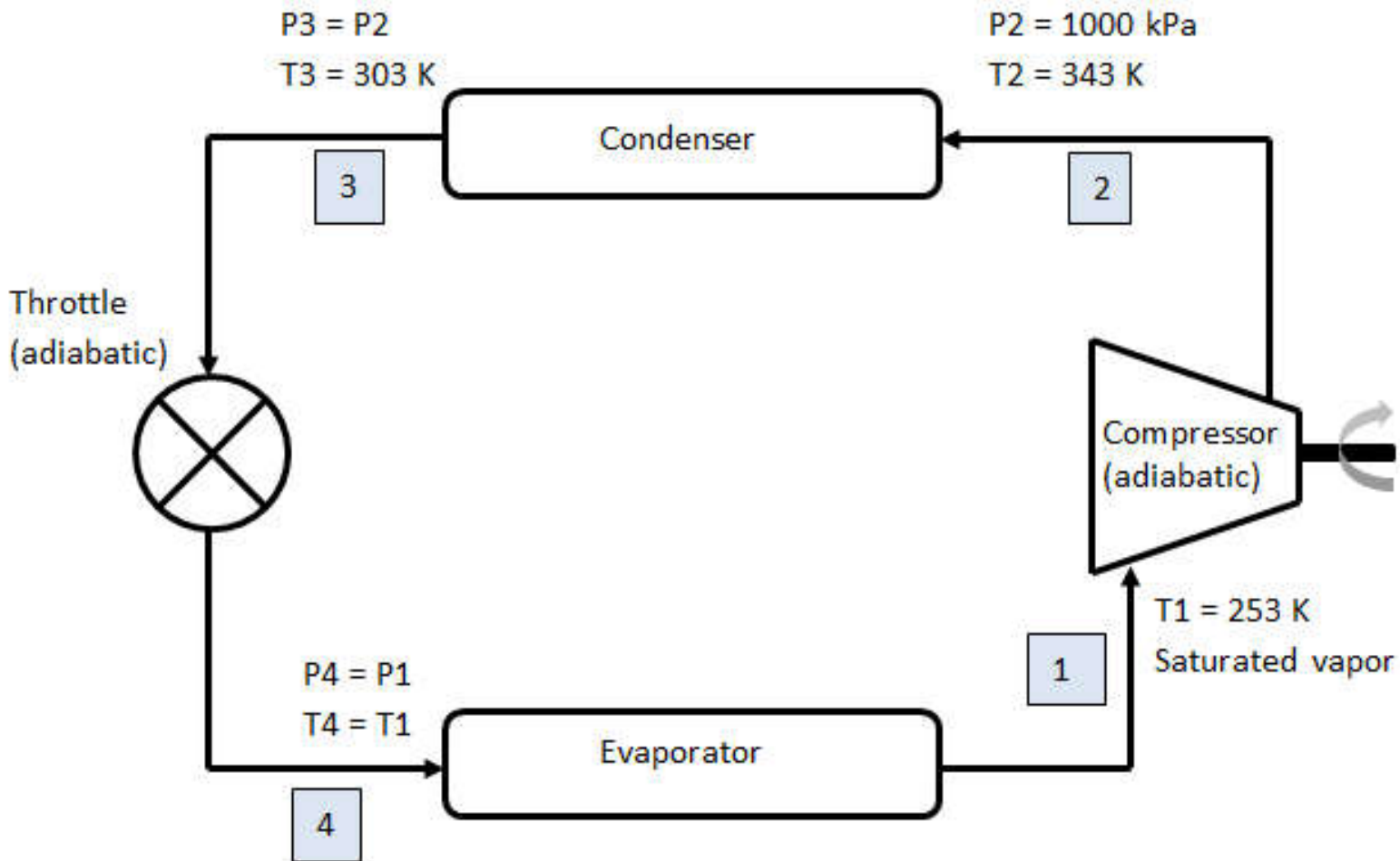


Analysis of a Vapor-Compression Refrigeration Cycle

▼ Introduction

This application analyzes the following refrigeration cycle, and calculates the coefficient of performance.



Additionally, the thermodynamic cycle will be plotted on a pressure-enthalpy-temperature chart.

The compressor, condenser, throttle and evaporator are analyzed in sequence with this equation, a statement of the conservation of energy,

$$q - w = \Delta h + \Delta KE + \Delta PE$$

where

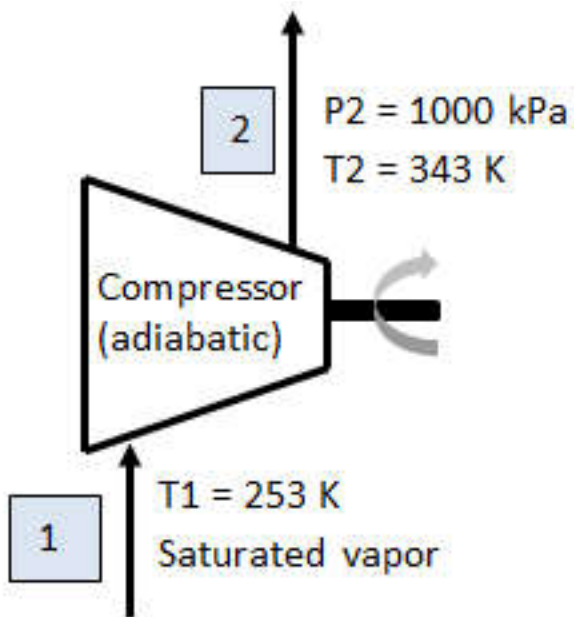
- w is the work done by the component
- ΔKE and ΔPE are the changes in kinetic and potential energy
- Δh is the change in specific enthalpy

- q is the heat transferred to the system

- > restart
- > with(ThermophysicalData) :
- with(Units[Standard]) :
- with(plots) :

▼ Compressor

Consider the energy flows in the compressor. For an adiabatic process, $q = 0$. Also $\Delta KE = 0$ and $\Delta PE = 0$. Hence $-w = \Delta h$



Enthalpies at points 1 and 2

- > $P2 := 1000 \cdot 10^3 \text{ Pa}$:

- > $h1 := \text{Property}(H, \text{temperature} = 253 \text{ K}, Q = 1, \text{R134a})$;

$$3.864615358 \cdot 10^5 \frac{\text{J}}{\text{kg}} \quad (2.1)$$

- > $h2 := \text{Property}(H, \text{temperature} = 343 \text{ K}, \text{pressure} = P2, \text{R134a})$;

$$4.518442441 \cdot 10^5 \frac{\text{J}}{\text{kg}} \quad (2.2)$$

The work done by the compressor (w)

- > $\text{workCompressor} := h1 - h2$

$$-65382.7083 \frac{\text{J}}{\text{kg}} \quad (2.3)$$

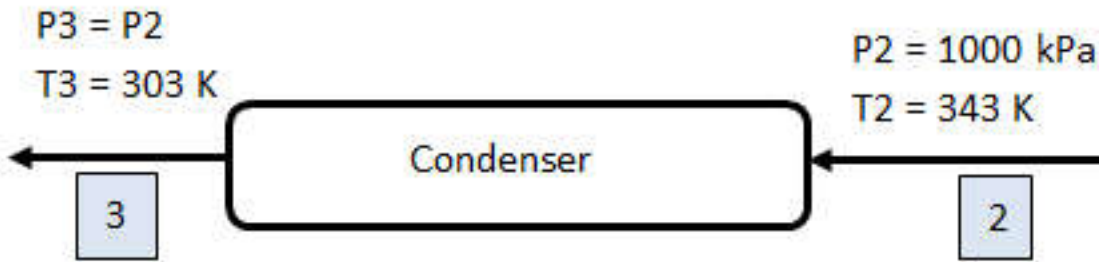
Pressure at point 1

- > $P1 := \text{Property}(P, \text{temperature} = 253 \text{ K}, Q = 1, \text{R134a})$

$$P1 := 1.318769284 \cdot 10^5 \text{ Pa} \quad (2.4)$$

▼ Condenser

For the condenser, $w = 0$, $\Delta KE = 0$ and $\Delta PE = 0$. Hence $q = \Delta h$



Enthalpy at point 3

> $h_3 := \text{Property}(H, \text{temperature} = 303 \text{ K}, \text{pressure} = P_2, \text{R134a})$

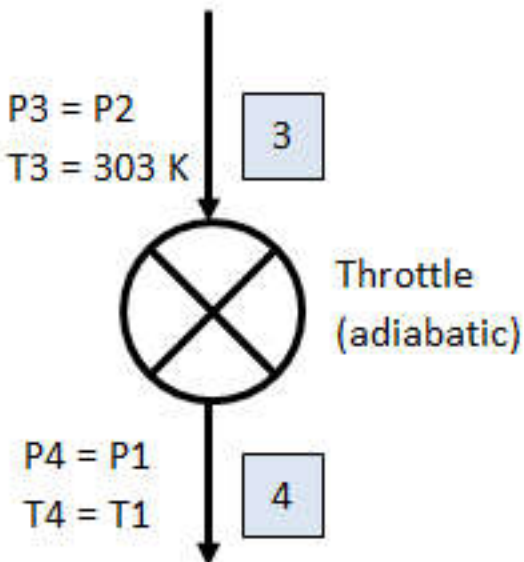
$$2.414995190 \cdot 10^5 \frac{\text{J}}{\text{kg}} \quad (3.1)$$

> $h_3 - h_2$

$$-2.103447251 \cdot 10^5 \frac{\text{J}}{\text{kg}} \quad (3.2)$$

▼ Throttle

For the throttle, $q = 0$, $w = 0$, $\Delta KE = 0$ and $\Delta PE = 0$. Hence $\Delta h = 0$



Enthalpy at point 4

> $h_4 := h_3$

$$2.414995190 \cdot 10^5 \frac{\text{J}}{\text{kg}} \quad (4.1)$$

Saturation pressure of R134a at 253 K

> P4 := P1

$$P4 := 1.318769284 \cdot 10^5 \text{ Pa}$$

(4.2)

Quality at P = press4 and H = h4

> Property(Q, pressure = P4, H = h4, R134a)

$$0.3194910312$$

(4.3)

▼ Evaporator

For the evaporator, $w = 0$, $\Delta KE = 0$ and $\Delta PE = 0$. Hence $q = \Delta h$



Heat extracted by evaporator

> heatEvaporator := h4 - h1

$$-1.449620168 \cdot 10^5 \frac{\text{J}}{\text{kg}}$$

(5.1)

▼ Coefficient of Performance

> $\frac{\text{heatEvaporator}}{\text{workCompressor}}$

$$2.217130807$$

(6.1)

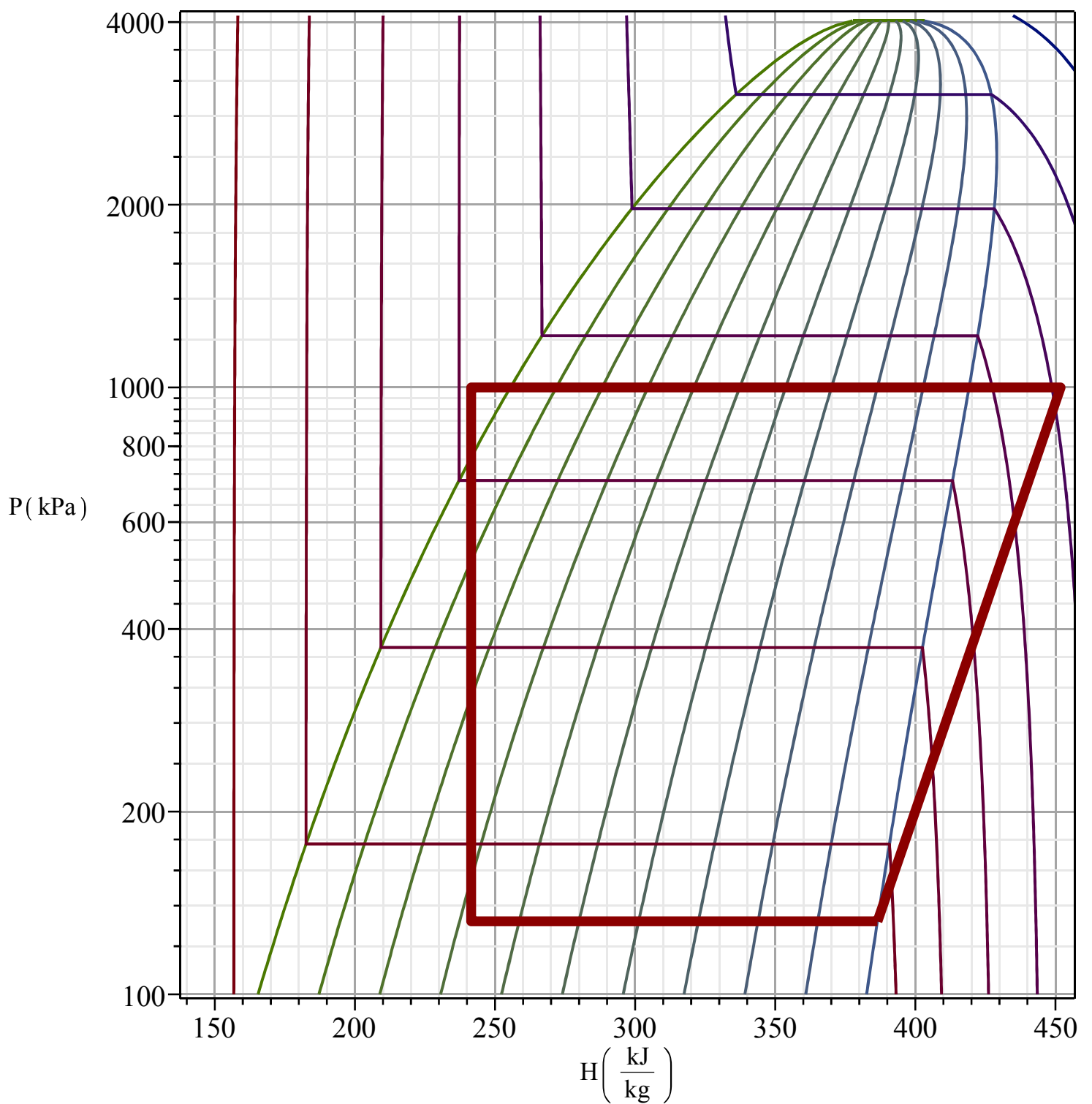
▼ Plot the Refrigeration Cycle on a P-h-T Chart

> phtChart := PHTChart(R134a, 100 kPa ..4100 kPa) :

> pts := convert~([([h1, P1]), [h2, P2], [h3, P2], [h3, P4], [h1, P1]], unit_free) :

> cycle := pointplot(0.001~pts, connect = true, color = "DarkRed", thickness = 5) :

> display(phtChart, cycle)



— quality 0.00
 — quality 1.00
 — isotherm 240.0 K
 — isotherm 380.0 K